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PRELIMINARY NOTE

Fluorination of Chlorofluoroethanes by Hydrogen [¹⁸F]-Fluoride in the Presence of a Chromia Catalyst

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SUMMARY

An 18 F tracer study of the fluorination of CCl₂FCClF₂ or C₂Cl₂F₄ isomers by hydrogen fluoride over a chromia catalyst, indicates that a surface fluoride species is involved. The interaction of HF with chromia is substantial, and evidence for three different fluoride species is presented.

Despite widespread interest in the catalytic fluorination of chlorofluoroethanes by hydrogen fluoride under heterogeneous conditions [1-4], little is known about the interactions which occur at the surface of the catalyst. We have obtained direct evidence for the involvement of a surface fluoride species from a fluorine-18 (t_1 =110 min) radiotracer study.

Flowing $H^{18}F$ over a pelleted, commercial chromia catalyst, contained in a Monel metal reactor equipped with an F.E.P. counting tube, at 623K for 0.5h, results in uptakes of ^{18}F activity which are equivalent to approximately 1 mmol $H^{18}F$ (g chromia)⁻¹. Flowing CCl_2FCClF_2 , He mixtures over chromia, labelled with ^{18}F in this way, for 0.5 h at 623K leads to the incorporation of 17-28% of the ^{18}F activity in the chlorofluoroethane mixtures produced. Two of the components of the mixtures are $[^{18}F]$ -CClF₂CClF₂ and $[^{18}F]$ -CCl₂FCClF₂, the specific activity of the former being greater than that of the latter. 64-71% of the activity

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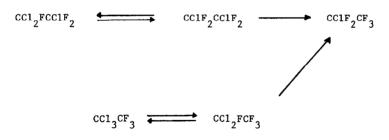
is retained by the solid. After extensive use, the fluorine and chlorine contents of the solid are 9.1 and 0.91 w/w% respectively, and its surface area has decreased from 66.5 to 22.0 m^2g^{-1} .

The behaviour of CC1_FCCIF₂ under these conditions, determined from 18 F tracer experiments and G.C. and 19 F n.m.r. analyses of product mixtures, is summarised in Scheme 1. The most important reactions at this temperature are 1, 2 and 3. Reaction 1 leads to $[^{18}$ F]-CCIF₂CCIF₂, and must

Scheme 1

involve a surface fluoride species. This reaction presumably provides the chloride species required for reaction 2. The sequence of reactions, 2 then 3, accounts for the labelling of $CCl_{2}FCClF_{2}$.

Similar behaviour is observed between $CC1F_2CC1F_2$ and $[^{18}F]$ -labelled catalyst at 698K. 19-22% of the ^{18}F originally present on the catalyst is incorporated in the chlorofluoroethane mixture produced. The $C_2C1_2F_4$ used contained 7.8% $CC1_2FCF_3$, and the behaviour of both compounds is summarised in Scheme 2. ^{18}F labelling of $Cc1F_2CF_3$ and $C_2C1_2F_4$ is observed, the specific activity of the former being the greater.



Scheme 2

We conclude that the reactions involved are true surface processes, and that the overall reactions are best described by non-synchronous fluorination and chlorination steps. There is no evidence for isomerisation reactions in contrast to previous suggestions [2,4].

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TABLE

H ¹⁸ F or HF food*	Flow time	Equivalent 18	Chromia count rate _1	ount rate _1	18 _F retained
TEECO		H''F uptake	count s	S	by chromia
cm ³ liquid	min.	mmol g ⁻¹	before HF flow	after HF flow	0 0
4.5	30	1.1	1110 ± 3	363 <u>+</u> 2	33
2.5	20	0.8	1058 + 3	437 ± 2	41
3.5	25	6.0	1861 + 4	952 <u>+</u> 3	51
4.0	25	1.0	2478 ± 5	1040 ± 3	42 [†]
4.0	25	1.25	1303 + 4	787 ± 3	60 [†]
4.0	25	0.5	2193 ± 5	1698 ± 4	77 [†]
4.0	25	0.7	1111 ± 3	397 ± 2	351
4.0	25	6.0	1271 ± 4	540 ± 2	43 [†]

* For a given experiment, $\mathrm{H}^{18}\,\mathrm{F}$ and HF feeds and flow times were identical.

 $^{\rm t}$ Sample pretreated with HF(g) prior to ${\rm H}^{18}{\rm F}$ flow.

The behaviour of HF towards the chromia catalyst is complex, and the active fluoride species which participates in the reactions described above, is one of three types which can be distinguished by ¹⁸F tracer experiments. Approximately 10-15% of the ¹⁸F activity transferred to chromia by H¹⁸F flow at 623K, is easily removed, for example by He flow for 0.5h at 623K. This fraction is considered to be present as weakly adsorbed HF. A greater proportion of ¹⁸F is removed by flowing inactive HF over $[^{18}F]$ -labelled catalyst and the results of a series of H¹⁸F then HF flow experiments on the same catalyst sample are shown in the Table. Although the behaviour is somewhat variable over the series, in each case a significant proportion of ¹⁸F is removed, either by displacement or by exchange with HF.

In the early stages, treatment of the catalyst with HF is accompanied by a small mass decrease (ca.3%), the condensation of aqueous HF downstream from the reactor, and the almost complete (95%) removal of surface hydroxyl groups, the latter being determined by ${}^{1}\text{H}/{}^{2}\text{H}$ exchange using mass spectrometric detection. Adsorption of HF, removal of bulk H₂O and the slow conversion of Cr^{III}-OH and Cr^{III}-O bonds to Cr^{III}-F, all appear to be important. The magnitude of ${}^{18}\text{F}$ uptake indicates that both surface and bulk changes occur. Comparison with the behaviour of CrF₃ towards H¹⁸F at 623K, indicates that the retained ${}^{18}\text{F}$, which is inert to exchange with HF, is directly bound to Cr^{III}.

A plausible model of the catalytic halogen exchange involves the formation of active sites during the early part of the catalyst's life, and an equilibrium between weakly adsorbed HF and catalytically active fluoride. The latter is lost, either by reaction with the adsorbed chlorofluorocarbon, or by a reaction which leads to the formation of Cr^{III}-F bonds.

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